## AMENDMENTS TO THE CLAIMS:

This listing of claims will replace all prior versions, and listings, of claims in the application:

## LISTING OF CLAIMS:

1. (currently amended) A method for controlling temperature in a boil-off gas in a liquefaction plant prior to compression, wherein boil-off gas originating from an LNG storage tank is compressed and at least partially condensed into a condensed boil-off gas, and wherein said condensed boil-off gas (LNG) is being returned to the storage tank, said method being characterized by comprising:

heat exchanging the boil-off gas with said LNG a condensed liquefied gas (LNG) through a wall separating said boil-off gas from said condensed liquefied gas (LNG), wherein the boil-off gas temperature is being lowered and said condensed liquefied gas LNG being fully evaporated as a fully evaporated LNG; and

controllably mixing said fully evaporated LNG with said boil-off gas.

2. (currently amended) The method of claim 1,  $\frac{1}{2}$  characterized by wherein said mixing of said fully evaporated LNG with said boil-off gas occurs upstream of said heat exchange.

- 3. (currently amended) The method of claim 1, characterized by wherein said mixing of said fully evaporated LNG with said boil-off gas during said compression.
- 4. (currently amended) The method of claim 1, characterized by wherein said mixing of said fully evaporated LNG with said boil-off gas following said compression.
- 5. (currently amended) The method of claim 1, characterized by : wherein maintaining a continuous flow of LNG and boil-off gas is maintained in said heat exchange exchanging step, whereby the LNG temperature is substantially constant.
- 6. (currently amended) The method of claim 1, characterized by wherein said controlling (25,60) of the mixing rate based on comprises the sub-step of comparing the temperature of the boil-off gas, downstream of said heat exchange, with [[a]] one or more predetermined temperature or range of temperatures.
- 7. (currently amended) An apparatus for controlling temperature in a boil-off gas in a liquefaction plant prior to compression, wherein boil-off gas from an LNG storage tank is fed via a boil-off gas feed line into at least one compressor (10) and where the compressed gas provided by the at least one compressor (10) is further fed into a heat exchanger (30) for at

least partial condensation <u>into a condensed boil-off gas (LNG)</u>, and where said condensed boil-off gas (LNG) is <del>being</del> returned to the storage tank via a return line, said apparatus <del>being</del> <del>characterized by</del> comprising:

- [[-]] a combined mist separator and heat exchanger (20) connected to the the boil-off gas feed line[[,]] at a point along the boil-off gas feed line between the LNG storage tank and the compressor (10);
- [[-]] a first conduit (22) fluidly connecting the return line for returning LNG to the storage tank and the combined mist separator and heat exchanger (20); and
- [[-]] a second conduit (26; 26'; 26") (26, 26', 26'')

  fluidly connecting the combined mist separator and heat exchanger

  (20) to the boil-off gas feed line[[;]],
- [[-]] wherein said first (22) and second (26;26'; 26")

  (26, 26', 26'') conduits being are fluidly connected via a cooler

  (24) in said combined mist separator and heat exchanger (20), and
- [[-]] wherein the cooler (24) comprises a wall configured to separate the boil-off gas from said condensed boil-off gas (LNG) and configured to transfer heat between the boil-off gas and said condensed boil-off gas (LNG) is heat exchanged against said cooler (24) prior to the boil-off gas being fed into said compressor (10).

- 8. (currently amended) The apparatus of claim 7, characterized by wherein said second conduit (26) fluidly connecting the combined mist separator and heat exchanger (20) to the boil-off gas feed line connects the cooler of said combined mist separator and heat exchanger (20) to said boil-off gas feed at a location upstream of said combined mist separator and heat exchanger (20).
- 9. (currently amended) The apparatus of claim 7, characterized by wherein said second conduit (26') fluidly connecting the combined mist separator and heat exchanger (20) connects to the boil-off gas feed line at a location after downstream of the first compression stage of said compressor (10).
- 10. (currently amended) The apparatus of claim 7, characterized by wherein said second conduit (26") fluidly connecting the combined mist separator and heat exchanger (20) to the boil-off gas feed line downstream of said compressor (10).
- 11. (currently amended) The apparatus of claim 7, <del>characterized by</del> further comprising:
- a control valve (25) in said first conduit (22), for controlling configured to control the LNG flow rate into the combined mist separator and heat exchanger (20).

- 12. (currently amended) The apparatus of claim 7, <del>characterized by</del> further comprising:
- a <u>first</u> control unit (60) connected to the control valve (25) and the boil-off gas feed line downstream of the combined mist separator and heat exchanger (20) and upstream of said compressor (10)[[,]]; and
- a  $\underline{\text{second}}$  control unit (61) connected to the control valve (25) and the boil-off gas feed line upstream of the cold box (30) and down stream of said compressor (10),  $\underline{\text{whereby}}$

wherein said first and second control units are configured to control the LNG flow rate into the combined mist separator and heat exchanger (20) is controllable based on the sensed temperatures of the boil-off gas in the feed line i) downstream said combined mist separator and heat exchanger (20) and ii) downstream said compressor (10).

13. (currently amended) The apparatus of claim 7, characterized in that wherein the combined mist separator and heat exchanger (20) additionally comprises a boil-off gas inlet (27), a chamber (29) and a drain (92) upstream of said cooler (24), and a mesh screen (28) between said heat exchanger (24) and an outlet (91),

whereby wherein the cooler (24) is configured to cool the boil-off gas is cooled by heat exchange with the cooler (24).